



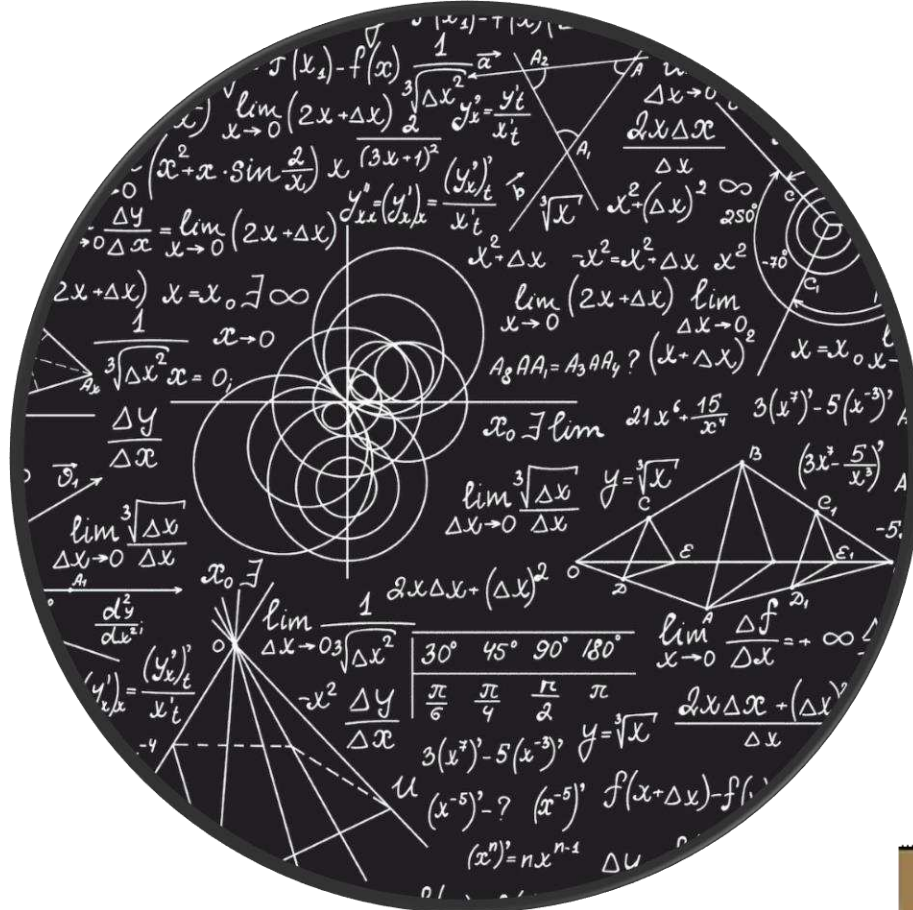
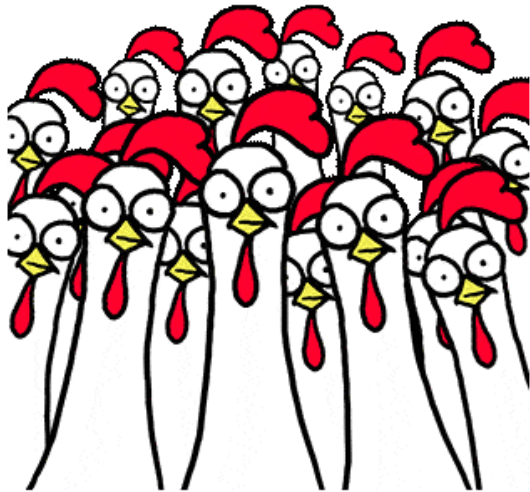
Mathematical Modeling: An Industrial Perspective

Ikenna Ireka (Ph.D.)

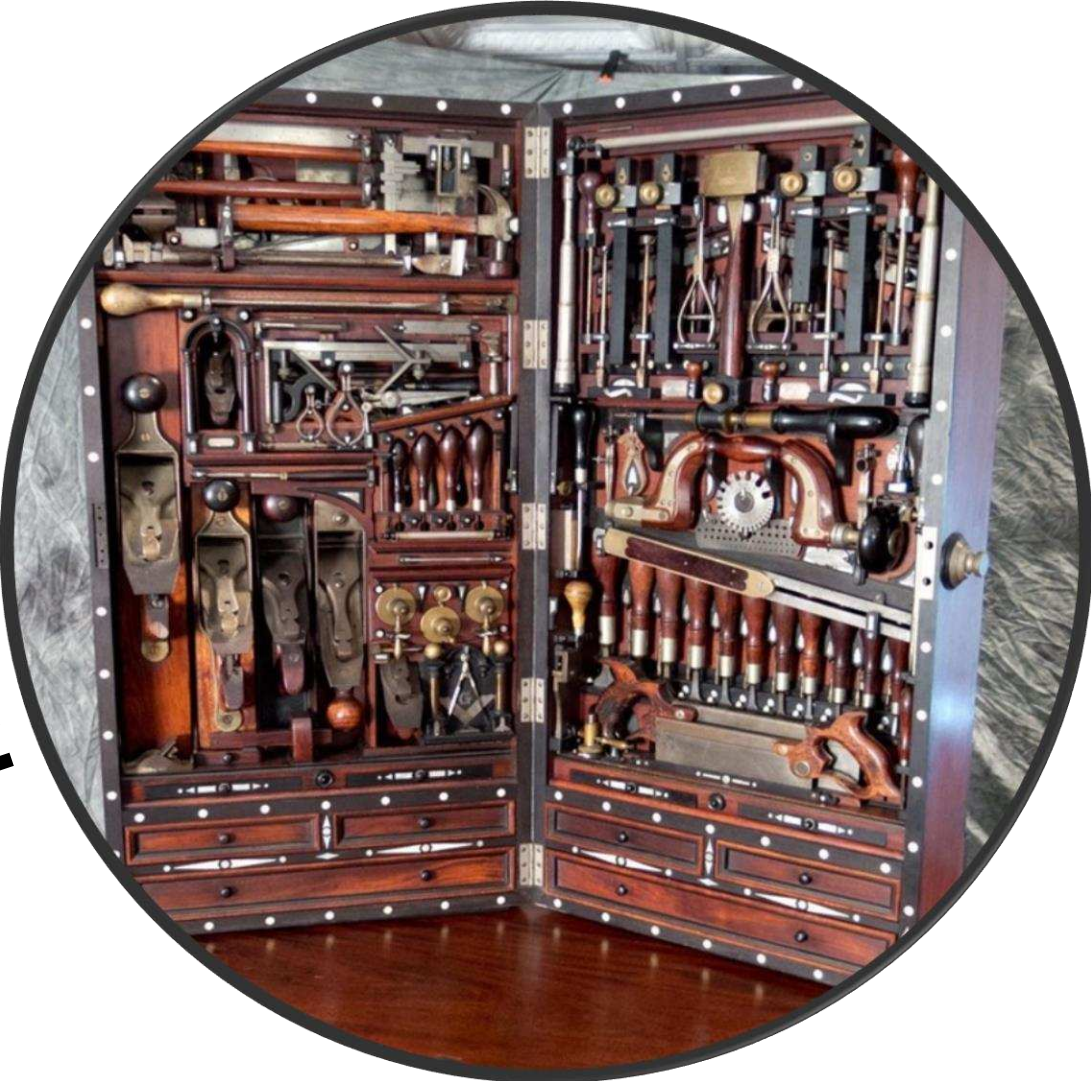
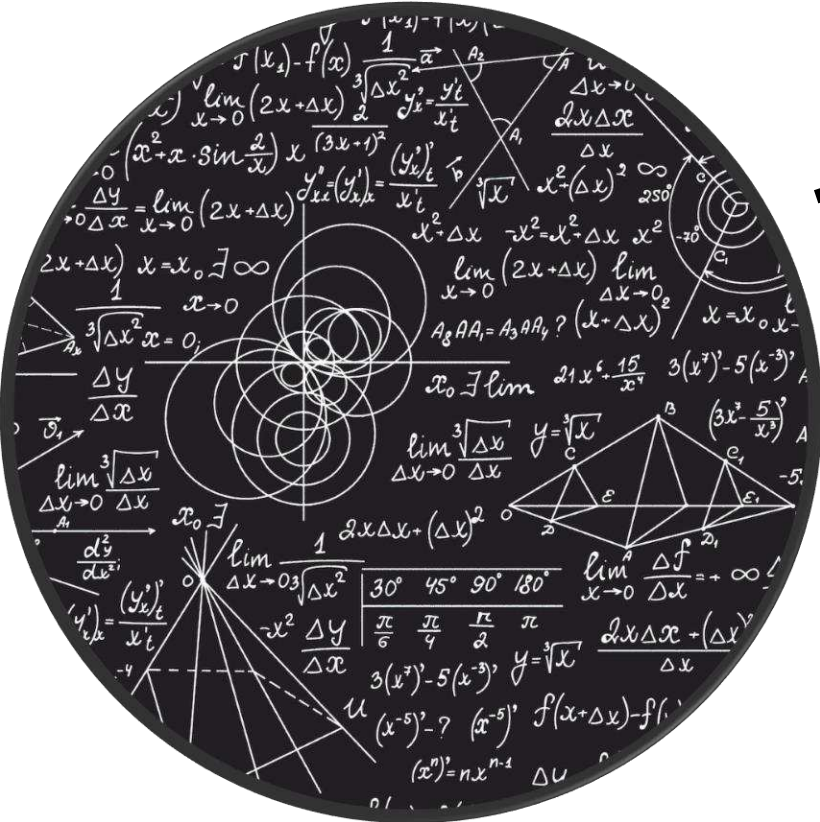
*International Conference and Advanced Workshop on Modelling and Simulation of Complex Systems,
May 2024, Obafemi Awolowo University Ile-Ife, Nigeria*

Journey of most STEM students

Freshmen / Jambites



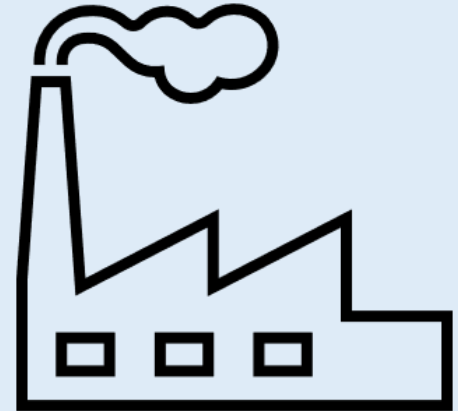
Toolbox



INDUSTRIAL CHALLENGES AN
OPPORTUNITY FOR APPLYING
MATHEMATICAL TOOLS

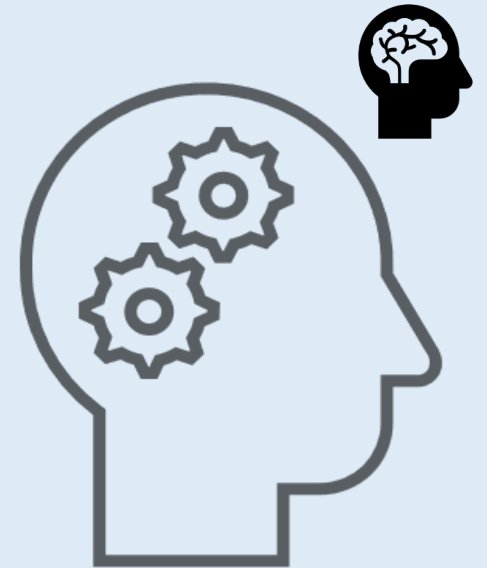
Some Challenges in the Industrial

- Optimize processes at minimal cost
- Remain Competitive at minimal cost
- Minimize experimental cost
- Optimize time to market
- Understand processing behavior of products
- Create/Design new products for competitive advantage
- ...

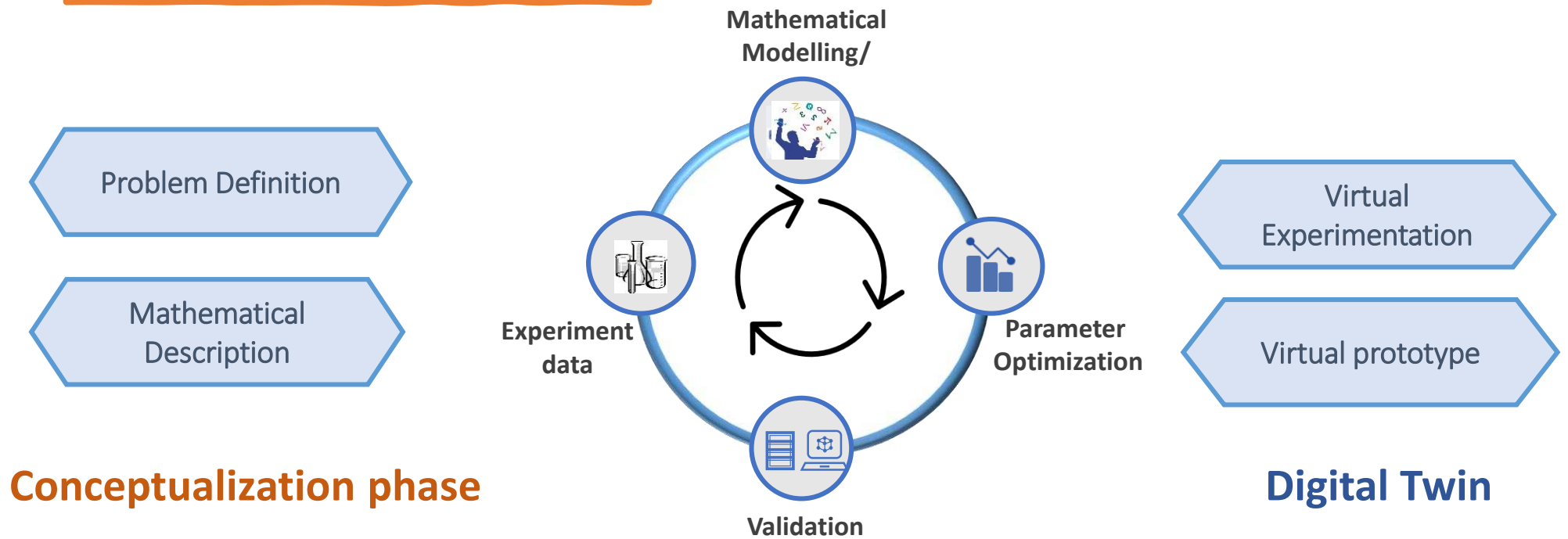


Resolving industrial challenges Mathematically

- Deterministic approach (known inputs)
 - Mathematical Modeling via physical laws (Differentia-Algebraic equations)
 - Numerical techniques
- Stochastic approach (randomness)
 - Data driven techniques
 - Machine Learning models
 - Forecasting (probabilistic models)
- Hybrid approach
 - Artificial Intelligence
 - AI-augmented simulations

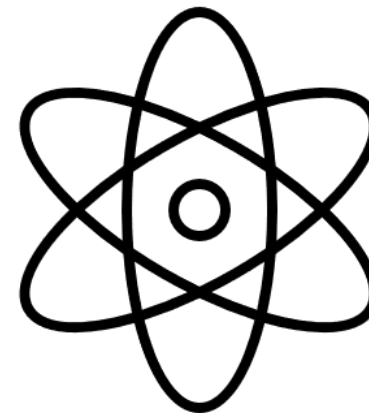
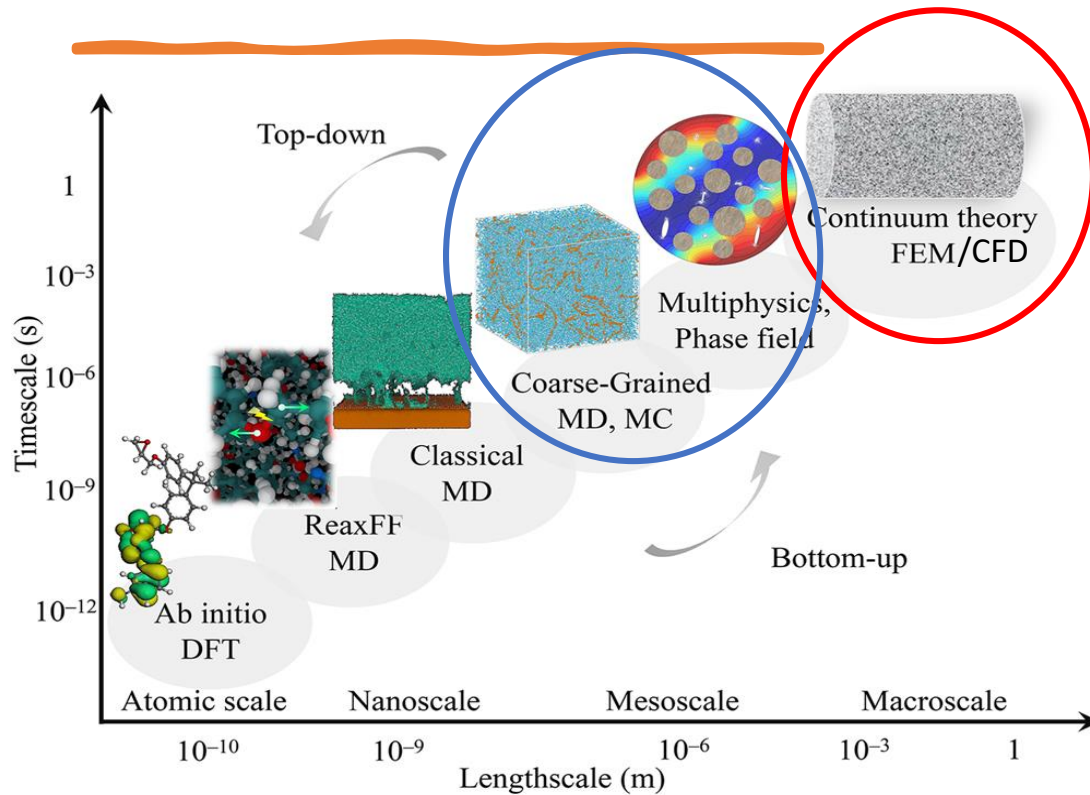


Modeling Industrial Problems



USE CASE
POLYMER INDUSTRY
(SIMULATION SCALE)

Multiscale system



[Multiscale mechanics and molecular dynamics simulations of the durability of fiber-reinforced polymer composites | Communications Materials \(nature.com\)](#)

USE CASES:
MATHEMATICAL METHODS IN
POLYMER INDUSTRY
(MACRO-SCALE SIMULATIONS)

Case 1: Some Questions in Polymer Injection molding

- How can we
 - understand the mold filling behavior in closed molds?
 - optimize process conditions and cycle time per molding process?
 - minimize defects in finished parts?
 - understand the material that is optimal for the mold of interest?
 - Efficiently design and maintain mold tooling to minimize failure?



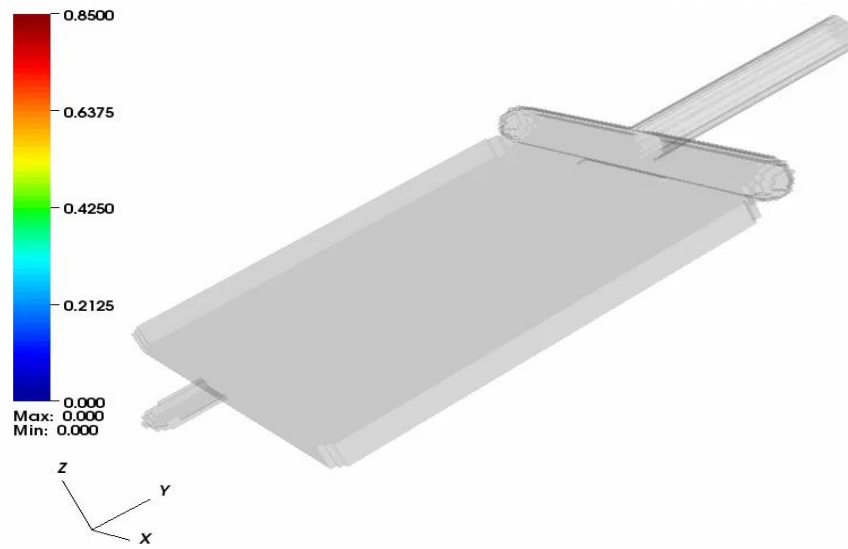
[Plastics Injection Mould Tool | Rutland Plastics](#)

Modeling Injection molding

The **Navier-Stokes Equations** subject to appropriate boundary conditions

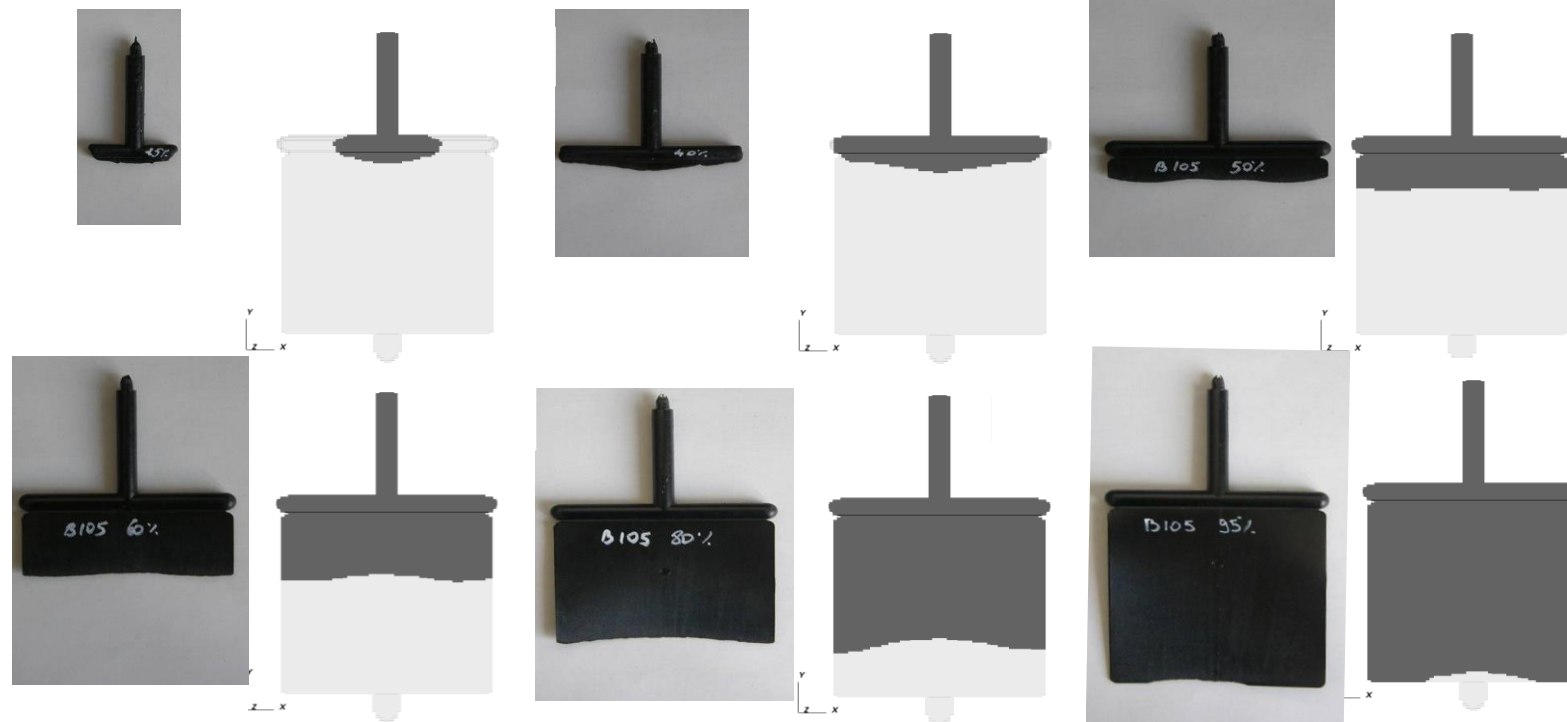
- **Conservation of mass** $\nabla \cdot \vec{v} = -\frac{1}{\rho} \left(\frac{\partial \rho}{\partial t} + \vec{v} \cdot \nabla \rho \right) = 0$ (incompressibility)
- **Conservation of linear momentum** $\frac{\partial \rho \vec{v}}{\partial t} + \nabla \cdot (\rho \vec{v} \vec{v}) = -\nabla p + \nabla \cdot \boldsymbol{\sigma} + \rho \mathbf{g}$
- **Conservation of energy:** $\rho C_p \left(\frac{\partial T}{\partial t} + \vec{v} \cdot \nabla T \right) = \nabla \cdot (\boldsymbol{\kappa} \nabla T) + \frac{1}{2} (\mu_{mix} \mathbf{D} : \mathbf{D})$

Case 1: Results Injection molding



Case 1: Results & Validation

Injection molding (3mm thickness)



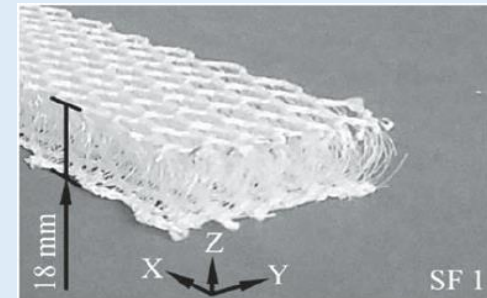
Case 1: Results & Validation

Injection molding (5mm thickness)



Case 2: Some Questions in Polymer Reinforced Injection molding

- What
 - is the effect of the reinforcing structure on the flow pattern?
 - regions of the structure will not be impregnated (wetted/dry) in the mold?
 - would be the optimal processing condition for such composite structure?
 - is the orientation of reinforcing chopped fiber glass in the formed part?



Sample Spacer fabrics used as inserts in the molding tools

Governing equations: Structural / chopped fiber Reinforced Injection molding

The Navier-Stokes-Brinkman Equations with appropriate boundary conditions

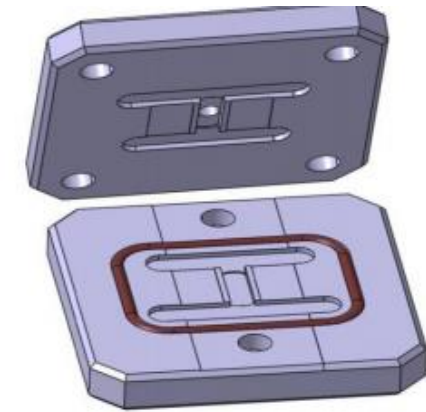
- Conservation of linear momentum $\frac{\partial \rho \vec{v}}{\partial t} + \nabla \cdot (\rho \vec{v} \vec{v}) = -\nabla p + \nabla \cdot \boldsymbol{\sigma} + \rho g - \mu_p \hat{K}^{-1} \vec{v}$

$$\hat{K}^{-1} \begin{cases} K^{-1}, & \text{porous region} \\ 0, & \text{non-porous region} \end{cases}$$

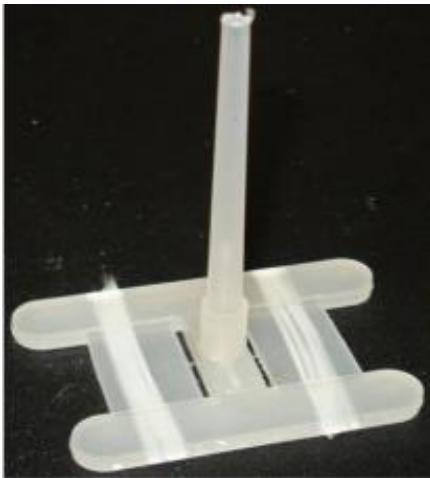
The Navier-Stokes-equations + Folgar-Tucker equations with appropriate boundary conditions

- Orientation tensor $\frac{dA}{dt} = W \cdot A - A \cdot W + \varepsilon (D \cdot A + A \cdot D - 2A^{(4)} : D) + 2D_r (I - 3A)$

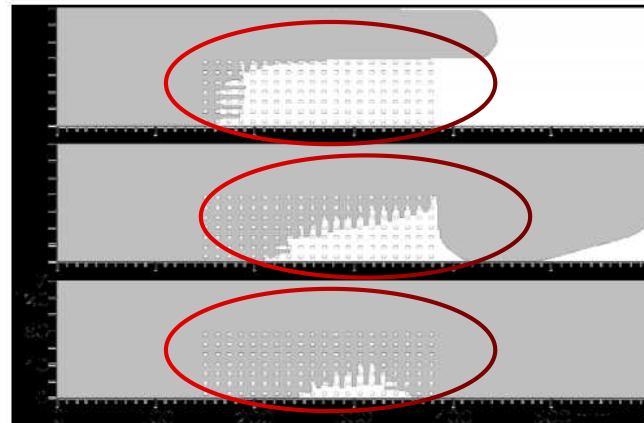
Case 2: Result, structural Reinforced Injection molding



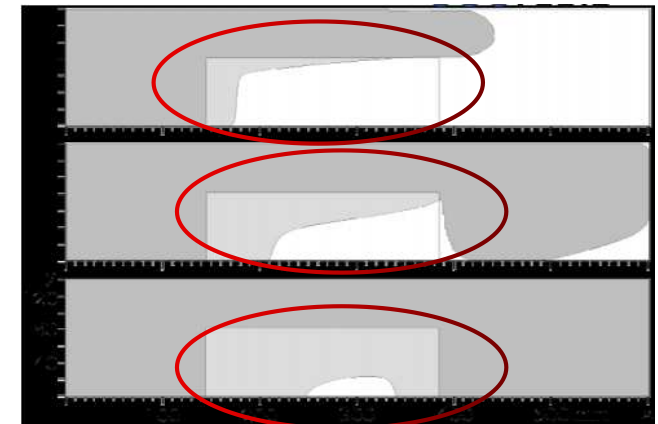
Finished Part



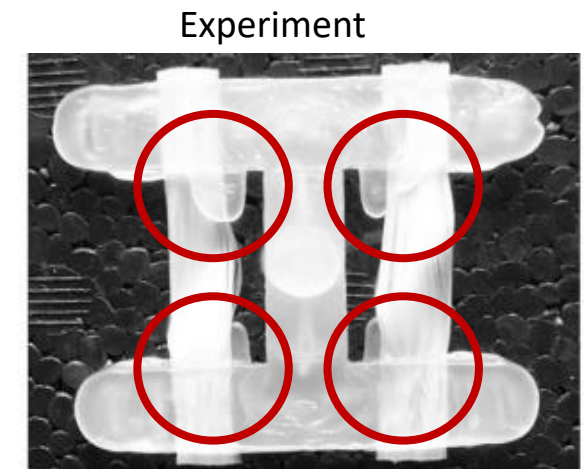
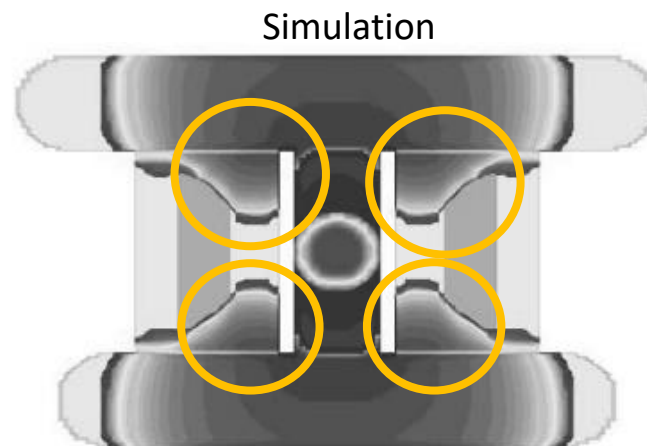
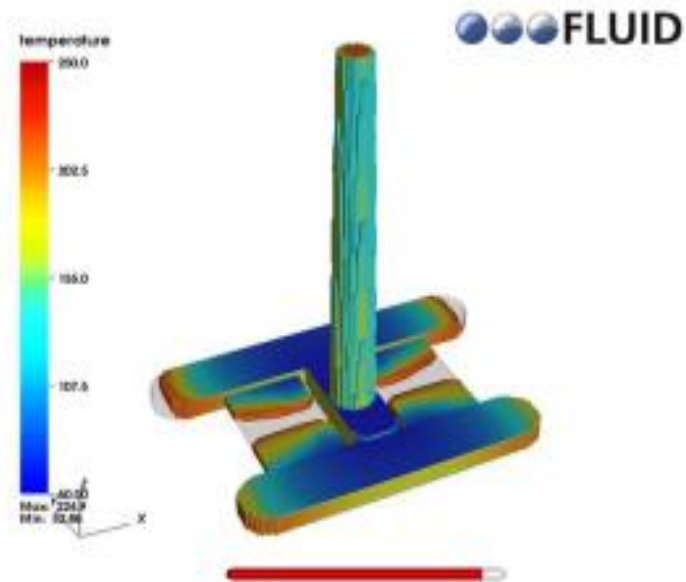
2D Micro pore simulation



2D Simulation with permeability tensor (K)



Case 2: Result, structural Reinforced Injection molding



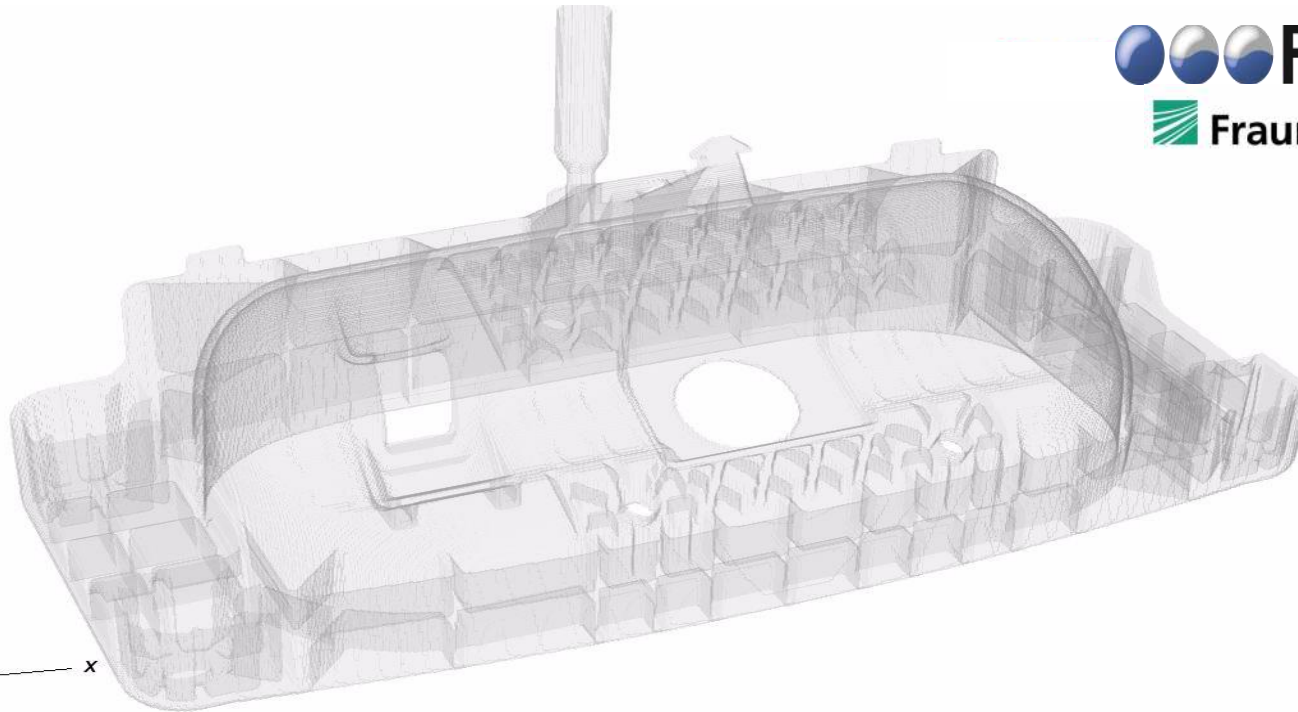
Case 2: Results

Orientation tensor of chopped fiber in reinforced Injection Molding

Vector
Var: FO_tensor
Constant.



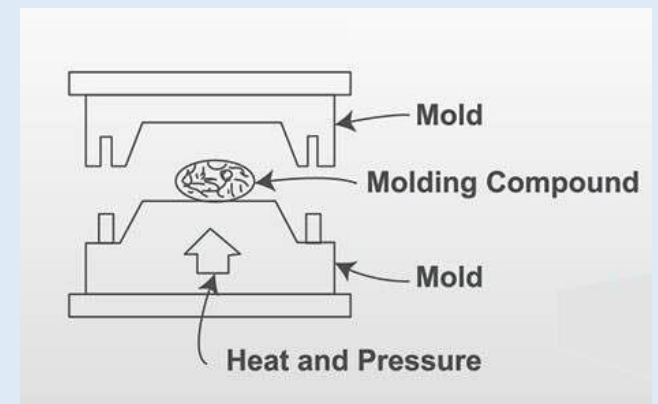
Max: 0.3333
Min: 0.3333



Case 3:

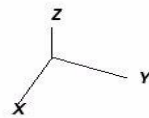
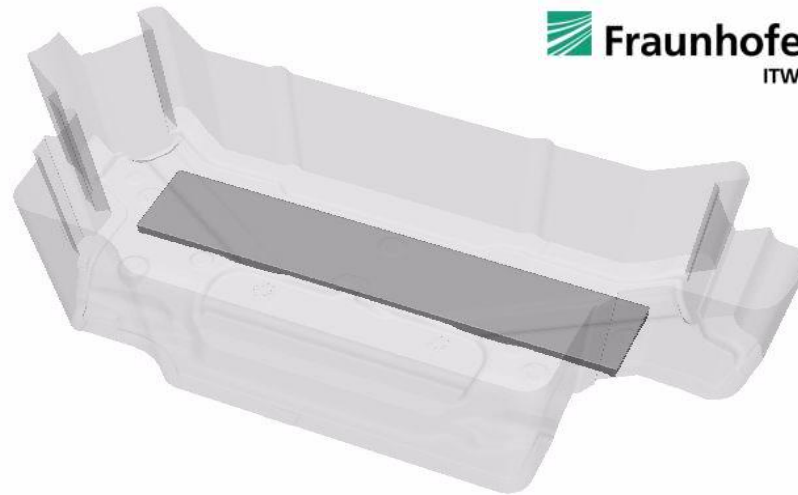
Some questions in Sheet Compression Molding (SMC)

- What amount of lumped polymer should be put in the mold,
- Where should the initial material (lump polymer) be placed in the mold for optimal distribution.
- What is the solidification time, i.e. how long do I need to wait for before opening the mold?
- What is the orientation of reinforcing chopped fiber glass?
- What is the distribution of the fiber in the finished part

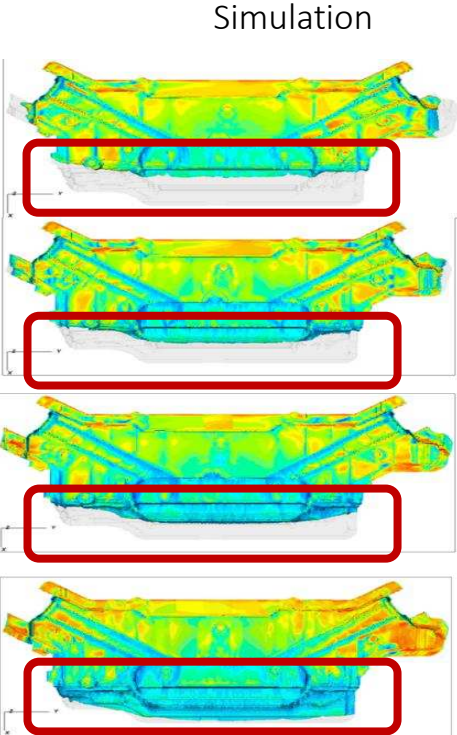
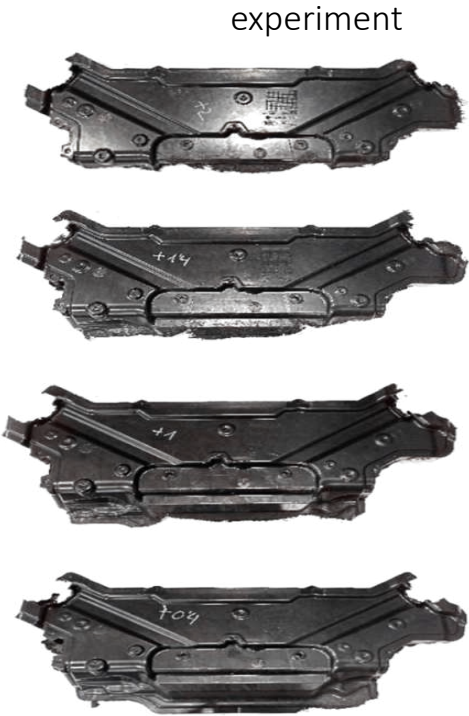


[The Complete Guide to Compression Molding - MDC Mould \(zjmdc.com\)](http://www.zjmdc.com)

Case 3: Results, Compression molding



Case 3: Results, Sheet Compression molding (SMC)



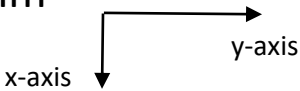
length of unfilled region in the mold

+2.0mm

+1.4mm

+1.0mm

+0.4mm



Case 4:

Reaction Injection Molding of Polyurethane (PUR) or Polyisocyanurate (PIR) foams

How can one

- minimize number of experimental trials
- enhance product development time
- understand the complex dynamics of expanding PUR foams in closed molds
- optimize processing (venting plan in automotive dashboard, optimal process temperature...)
- optimize mold design
- ...

Application of reaction Injection molding of Polyurethane foams

Automotive



Housing



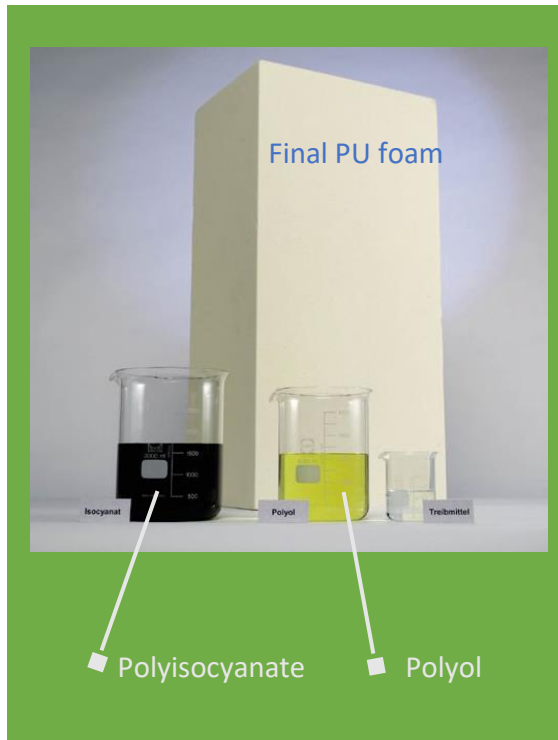
Appliances



Comfort



Quick overview: Chemistry of PUR/PIR foams

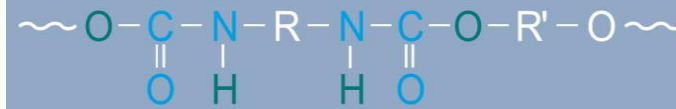


Polyisocyanate

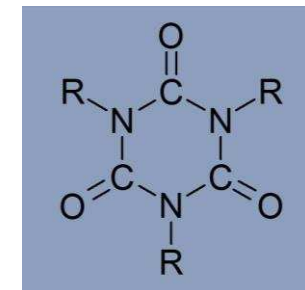
Polyol

Blowing agent(s)

catalysts

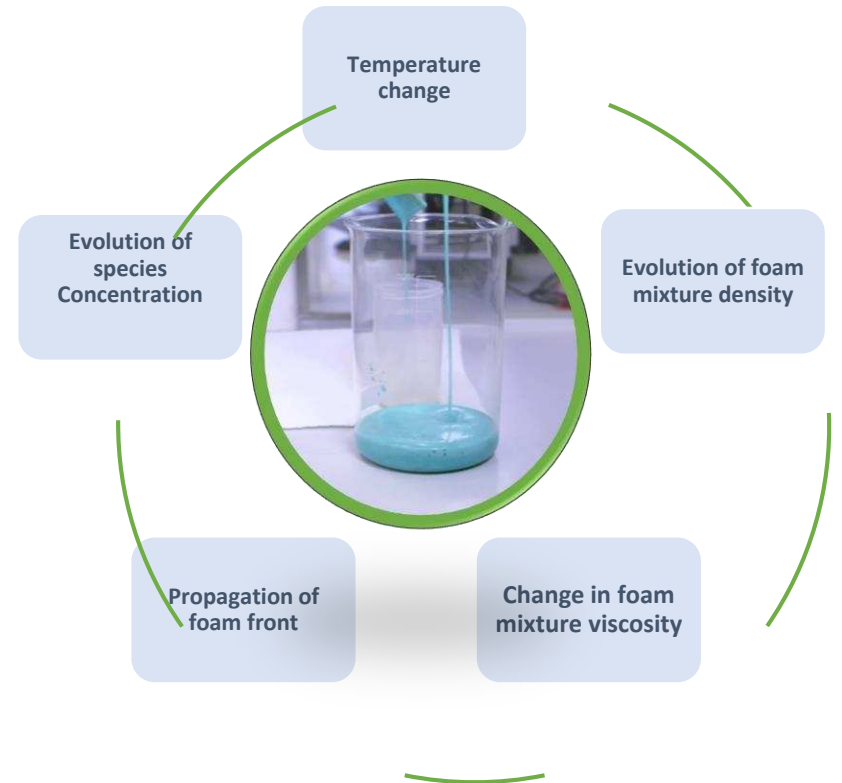


Polyurethane foams



Polyisocyanurate foam

PUR Foam expansion experiment: Observed Physics



Modeling Reaction Injection Molding of Polyurethane (PUR)foams

The Navier-Stokes Equations + additional equations for specie transport

- Conservation of energy:**

$$\rho C_p \left(\frac{\partial T}{\partial t} + v \cdot \nabla T \right) = \nabla \cdot (\kappa \nabla T) + \frac{1}{2} (\mu_{mix} \mathbf{D} : \mathbf{D}) + S_R$$

$$(-\Delta H_{OH}, -\Delta H_w, \Delta H_{PIR}) \cdot \left(\frac{dC_{OH}}{dt}, \frac{dC_w}{dt}, \frac{dC_{PIR}}{dt} \right)^T$$
- Equation for Concentration of CO₂:**

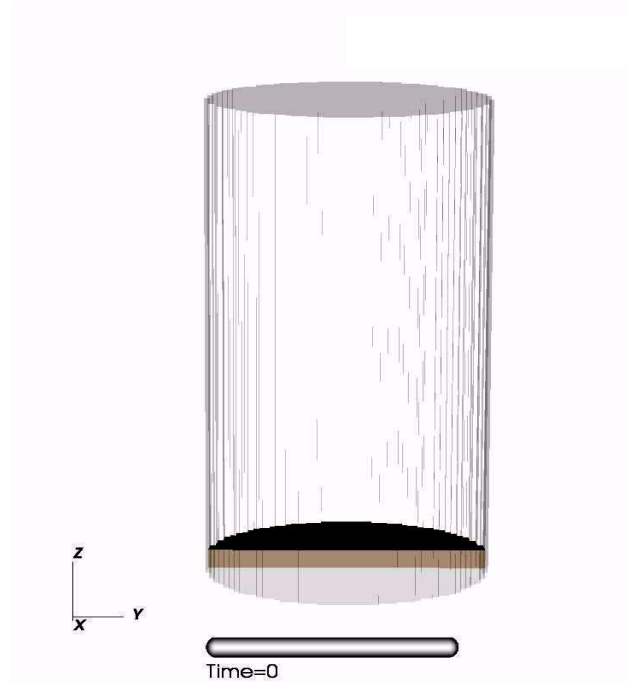
$$\frac{\partial C_{CO_2}}{\partial t} + \nabla \cdot (v C_{CO_2}) = K_w C_{NCO} C_w,$$
- Equation for Water and Polyol concentrations:**

$$\frac{\partial C_i}{\partial t} + \nabla \cdot (v C_i) = -K_i C_i C_{NCO}$$

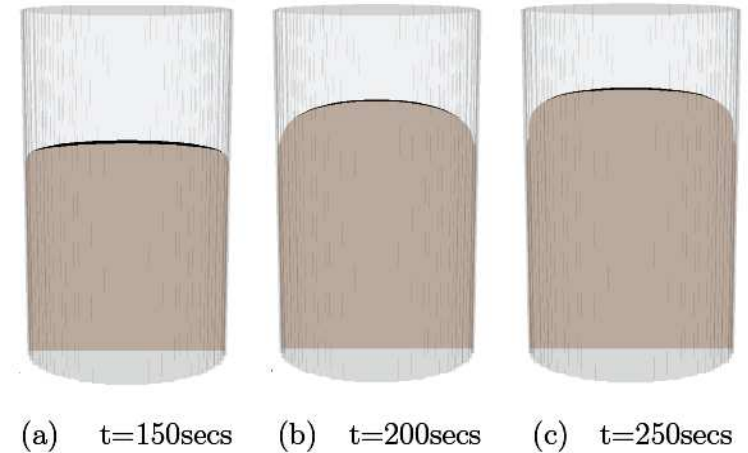
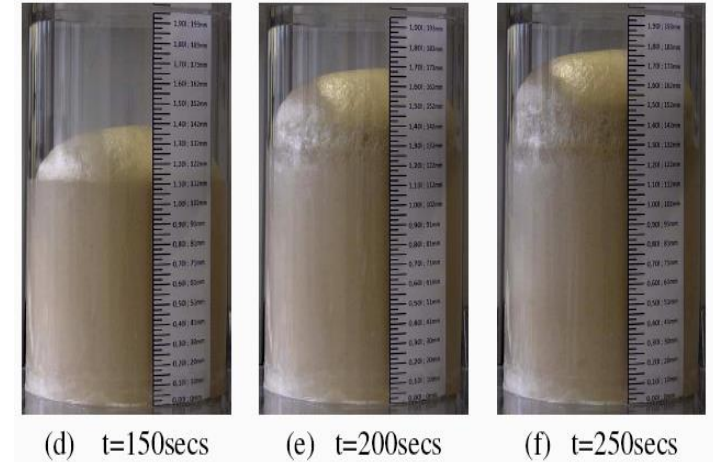
$$K_i = A_i e^{-\frac{E_i}{RT}} \quad \text{and} \quad i = OH, w$$
- Equation for NCO Concentration**

$$\frac{\partial C_{NCO}}{\partial t} + \nabla \cdot (v C_{NCO}) = -(K_w C_w + K_{OH} C_{OH}) * C_{NCO}$$

Case 2: Result & Validation, PUR Foam expansion

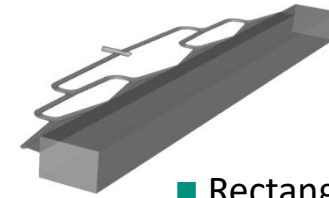


Experiment

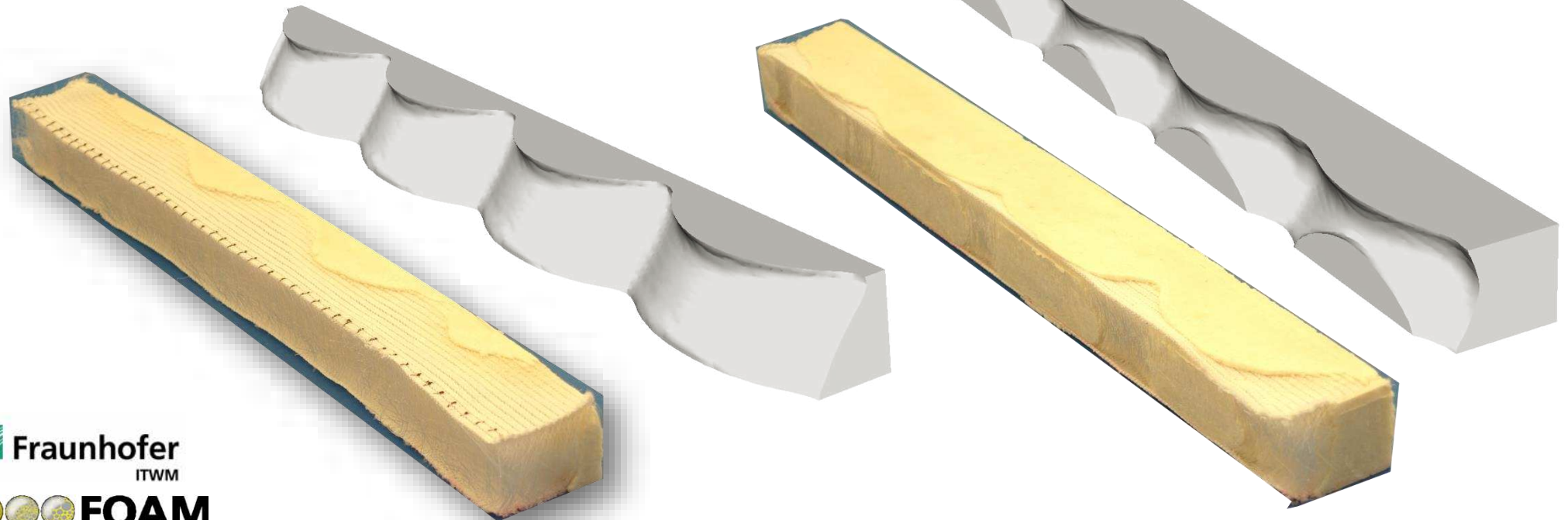


Simulation

Case 2: Result, PUR foam Structural Reinforced Reaction Injection molding



■ Rectangular geometry:

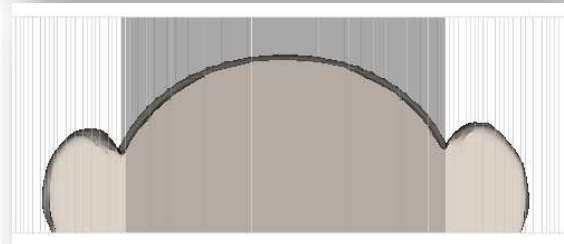
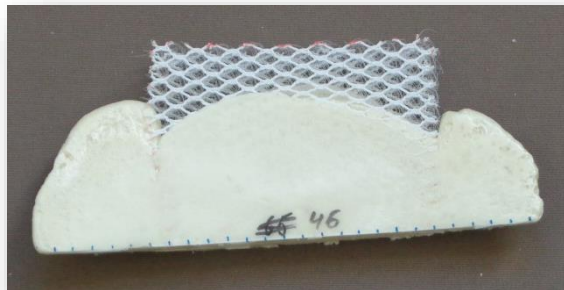


Case 2: Result, PUR foam Structural Reinforced Reaction Injection molding

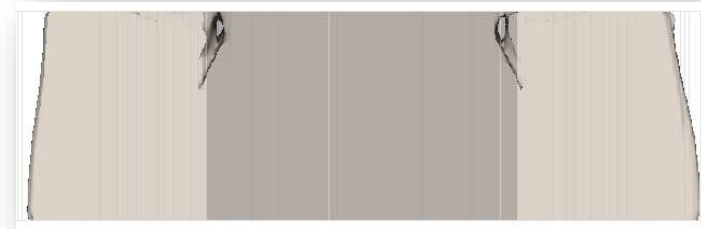
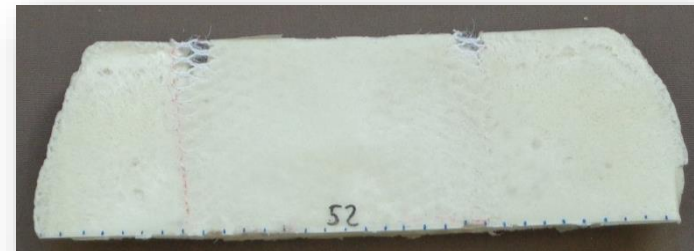


■ Wave geometry:

20 g

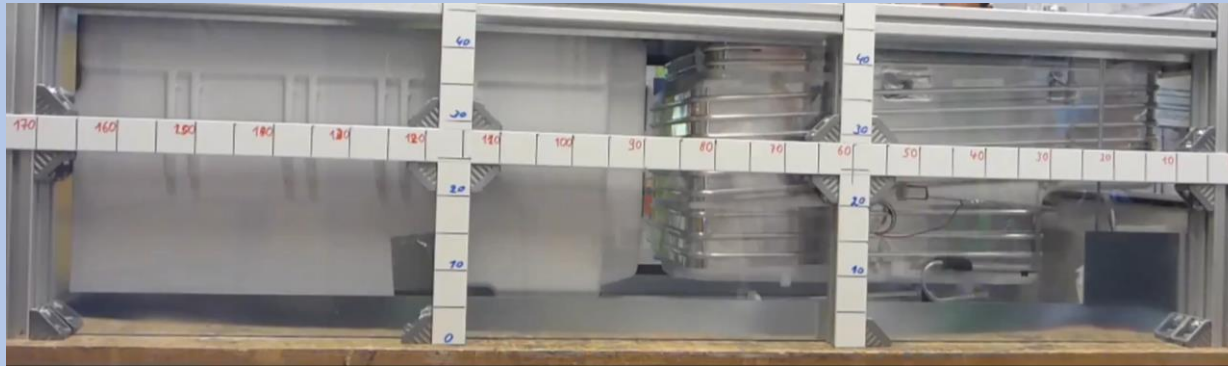


30 g



Foaming Simulation of Refrigerator cabinet

Validation with experiment



Time: 0.0 s

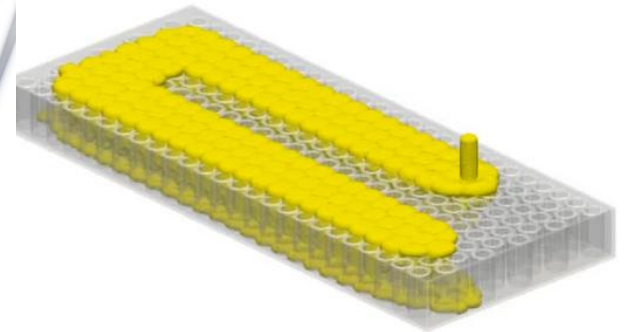
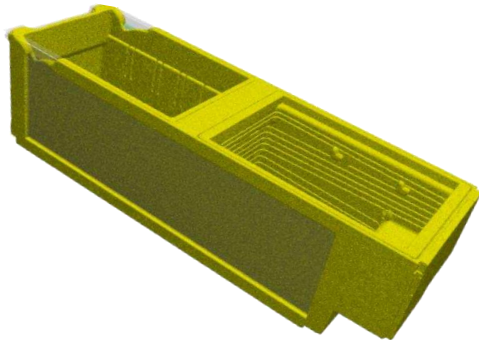
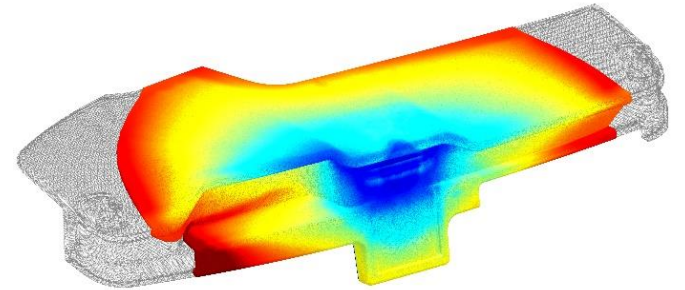
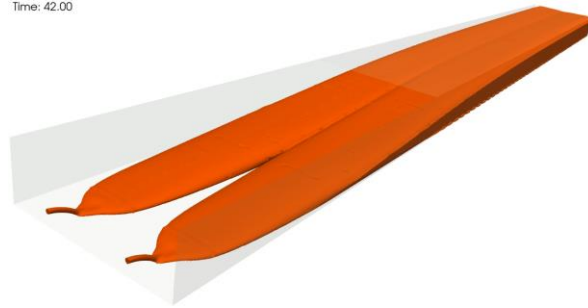


Simulation aided prototyping

Conclusion



Time: 42.00



Conclusion



Industrial virtual material prototyping via Mathematical concepts

- Interaction with domain experts
- Experimentation
- Model development
- Parameter optimization
- Model validation (numerical simulations simple cases)
- Simulation of real industrial case
- Virtual prototype & experimentation for process optimization (Digital twin)

THANK YOU
FOR YOUR ATTENTION

Introduction to Complex Fluids

Ikenna Ireka (*Ph.D.*)



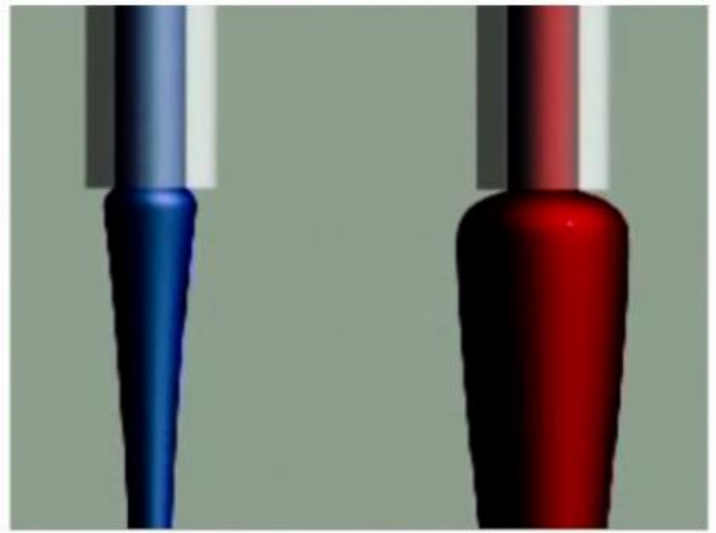
Overview

- Newtonian vs Non-Newtonian (complex) fluids
 - Complex rheological models
 - Generalized Newtonian fluids
 - Viscoelastic fluids
 - Chemorheological fluids (Polyurethane foams)
- The Navier Stokes Equation
- The Navier-Stokes Brinkman Equations

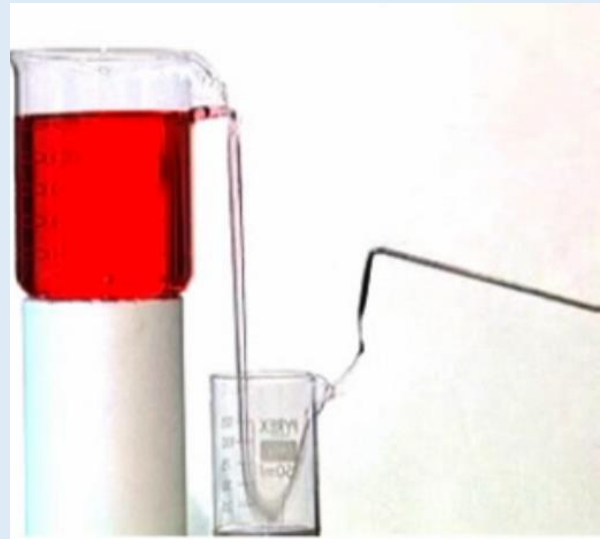
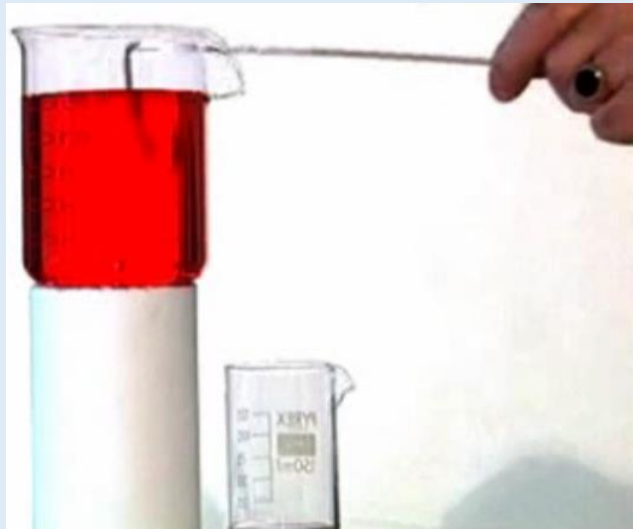
Simple Fluids



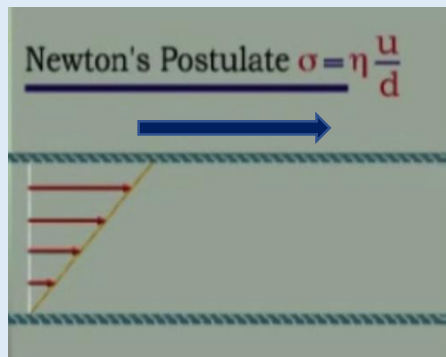
Simple vs Complex Fluids



Complex Fluids



Newtonian Fluids



σ is the shear stress

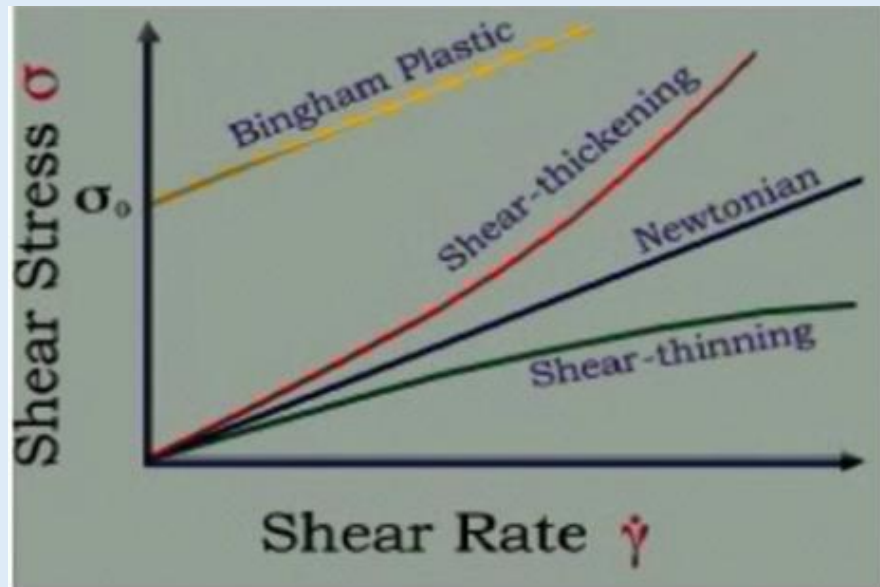
$\frac{u}{d}$ is the velocity gradient

η is the coefficient of viscosity

Table 1.1: Temperature dependent viscosity models

Reynold's model	$\eta(T) = \eta_0 \exp(-BT)$
Vogel's model	$\eta(T) = \eta_0 \exp\left(\frac{B}{T-T_0}\right)$
Arrhenius model	$\eta(T) = \eta_0 \exp(E/RT)$
Nahme model	$\eta(T) = \eta_0 \exp\left(\frac{T-T_0}{T_0}\right)$
William-Landel-Ferry (WLF) model	$\eta(T) = \eta_0 \exp\left(\frac{-C_1(T-T_0)}{C_2+T-T_0}\right)$
Fulcher model	$\log_{10}(\eta(T)) = -A + \frac{B \times 10^3}{T-T_0}$

Stress strain Curves: Simple vs Complex Fluids



- Viscoelasticity
- Variable Viscosity
- Normal Stresses
- Extensional Viscosity
- Thixotropy and Anti-Thixotropy
- Other Effects

The Navier-Stokes Equations

The **Navier-Stokes Equations** subject to appropriate boundary conditions

- **Conservation of mass**
$$\nabla \cdot \vec{v} = -\frac{1}{\rho} \left(\frac{\partial \rho}{\partial t} + \vec{v} \cdot \nabla \rho \right)$$
- **Conservation of linear momentum**
$$\frac{\partial \rho \vec{v}}{\partial t} + \nabla \cdot (\rho \vec{v} \vec{v}) = -\nabla p + \nabla \cdot \mathbf{T} + \mathbf{F}$$
- **Conservation of energy:**
$$\rho C_p \left(\frac{\partial T}{\partial t} + \vec{v} \cdot \nabla T \right) = \nabla \cdot (\boldsymbol{\kappa} \nabla T) + \frac{1}{2} (\mu_{mix} \mathbf{D} : \mathbf{D})$$

Constitutive relations

- Newtonian $\mathbf{T} = 2\eta\mathbf{D}$, with, $\mathbf{D} = \frac{1}{2} [\nabla\mathbf{v} + (\nabla\mathbf{v})^T]$.

- Generalized Newtonian** $\mathbf{T} = 2\eta(\dot{\gamma}) \mathbf{D}$.

- Power law Model $\eta = K\dot{\gamma}^{n-1}$,

if $n < 1$	$\lim_{\dot{\gamma} \rightarrow 0} \eta(\dot{\gamma}) = \infty$	$\lim_{\dot{\gamma} \rightarrow \infty} \eta(\dot{\gamma}) = 0$,
if $n > 1$	$\lim_{\dot{\gamma} \rightarrow 0} \eta(\dot{\gamma}) = 0$	$\lim_{\dot{\gamma} \rightarrow \infty} \eta(\dot{\gamma}) = \infty$.

- Prandtl-Eyring $\eta = \eta_0 \frac{\sinh^{-1}(\lambda\dot{\gamma})}{\lambda\dot{\gamma}}$, $\lim_{\dot{\gamma} \rightarrow 0} \eta(\dot{\gamma}) = \eta_0$, $\lim_{\dot{\gamma} \rightarrow \infty} \eta(\dot{\gamma}) = 0$.

More generalized Newtonian fluids

- Powell-Eyring model

$$\eta = \eta_\infty + (\eta_0 - \eta_\infty) \frac{\sinh^{-1}(\lambda \dot{\gamma})}{\lambda \dot{\gamma}}, \quad \frac{\eta - \eta_\infty}{\eta_0 - \eta_\infty} = \frac{\sinh^{-1}(\lambda \dot{\gamma})}{\lambda \dot{\gamma}}, \quad \lim_{\dot{\gamma} \rightarrow 0} \eta = \eta_0 \quad \text{and} \quad \lim_{\dot{\gamma} \rightarrow \infty} \eta = \eta_\infty.$$
- Cross model

$$\frac{\eta - \eta_\infty}{\eta_0 - \eta_\infty} = \frac{1}{1 + (\lambda \dot{\gamma})^m}, \quad \text{if } m < 1 \quad \lim_{\dot{\gamma} \rightarrow 0} \eta(\dot{\gamma}) = \eta_0 \quad \lim_{\dot{\gamma} \rightarrow \infty} \eta(\dot{\gamma}) = \eta_\infty,$$

$$\frac{\eta_0 - \eta}{\eta - \eta_\infty} = (\lambda \dot{\gamma})^m, \quad \text{if } m > 1 \quad \lim_{\dot{\gamma} \rightarrow 0} \eta(\dot{\gamma}) = \eta_\infty \quad \lim_{\dot{\gamma} \rightarrow \infty} \eta(\dot{\gamma}) = \eta_0,$$
- Sisko model

$$\eta = \eta_\infty + K \dot{\gamma}^{n-1}.$$
- Carreau-Yasuda model

$$\frac{\eta - \eta_\infty}{\eta_0 - \eta_\infty} = [1 + (\lambda \dot{\gamma})^c]^{(n-1)/c}, \quad c = 2 \text{ (Carreau Model)}$$